AMENDMENTS TO THE CLAIMS

Please amend the claims as follows.

1. (Previously Presented) A composition comprising a polymer blend of:

- a) a first random copolymer of propylene and at least one non-propylene C₂-C₂₀ α-olefin, said first random copolymer having a propylene content of above 90 up to about 99.5 weight percent, a melting point of above 116°C to about 145°C and which constitutes from about 60 weight percent to about 95 weight percent of the composition, and
- b) a second random copolymer of propylene and at least one non-propylene C₂-C₂₀ α-olefin, said second random copolymer having a propylene content of above 85 up to about 97 weight percent, but less than the propylene content of the first random copolymer, a melting point from about 70°C to no more than 116°C and which constitutes from about 5 weight percent to about 40 weight percent of the composition,
- wherein said polymer blend includes a fraction soluble in xylene at 20°C, determined at 20°C and 5 days settling time, the xylene soluble fraction having a weight average molecular weight of more than 100 kg/mol and an intrinsic viscosity of above about 1.0 dl/g.
- 2. (Original) The composition of claim 1 wherein said xylene soluble fraction has a weight average molecular weight of above about 150 kg/mol.
- 3. (Previously Presented) The composition of claim 1 wherein said xylene soluble fraction has a weight average molecular weight of above about 200 kg/mol.
- 4. (Previously Presented) The composition of claim 1 wherein said xylene soluble fraction has a weight average molecular weight of above about 300 kg/mol.
- 5. (Original) The composition of claim 1 wherein said xylene soluble fraction has an intrinsic viscosity of above about 1.3 dl/g.

6. (Original) The composition of claim 1 wherein said xylene soluble fraction has an intrinsic viscosity of above about 1.6 dl/g.

- 7. (Original) The composition of claim 1 wherein said xylene soluble fraction has an intrinsic viscosity of above about 2.0 dl/g.
- 8. (Currently Amended) The composition of claim 1,[[claims 1,]] wherein the polymer blend includes from 3 to 30 weight percent of ultra low crystallinity fractions, said ultra low crystallinity fractions being defined as the difference between the amount of xylene soluble components as determined at 20°C and 2 hours settling time and the amount of xylene soluble components as determined at 20°C and 5 days settling time.
- 9. (Original) The composition of claim 1 having a melt flow rate at 230°C and 2.16 kg of above 2 to about 15 g/10 min.
- 10. (Currently Amended) The composition of claim 1,[[claims 1]] wherein both random copolymers of the polymer blend were prepared by means of a metallocene catalyst.
- 11. (Original) A film having at least one layer fabricated from the composition of claim 1.
- 12. (Original) The film of claim 11, wherein the amount of hexane extractable fraction of the film layer comprises no more than about 3.0 weight percent.
- 13. (Previously Presented) A composition comprising a polymer blend of:
 - a) a first random copolymer of propylene and ethylene, said first random copolymer having a propylene content of above 90 up to about 99.5 weight percent and a melting point of above 116°C to about 145°C, and which constitutes from about 60 weight percent to about 95 weight percent of the composition, and

b) a second random copolymer of propylene and ethylene, said second random copolymer having a propylene content of above 85 up to about 97 weight percent, but less than the propylene content of the first random copolymer, a melting point from about 70°C to no more than 116°C, and which constitutes from about 5 weight percent to about 40 weight percent of the composition,

wherein said polymer blend includes a fraction soluble in xylene at 20°C, determined at 20°C and 5 days settling time, the xylene soluble fraction having a weight average molecular weight of more than 100 kg/mol and an intrinsic viscosity of above about 1.0 dl/g.

- 14. (Previously Presented) The composition of claim 13 wherein said xylene soluble fraction has a weight average molecular weight of above about 150 kg/mol.
- 15. (Original) The composition of claim 13 wherein said xylene soluble fraction has a weight average molecular weight of above about 200 kg/mol.
- 16. (Previously Presented) The composition of claim 13 wherein said xylene soluble fraction has a weight average molecular weight of above about 300 kg/mol.
- 17. (Original) The composition of claim 13 wherein said xylene soluble fraction has an intrinsic viscosity of above about 1.3 dl/g.
- 18. (Original) The composition of claim 13 wherein said xylene soluble fraction has an intrinsic viscosity of above about 1.6 dl/g.
- 19. (Original) The composition of claim 13 wherein said xylene soluble fraction has an intrinsic viscosity of above about 2.0 dl/g.

20. (Original) The composition of claim 13, wherein the polymer blend includes from 3 to 30 weight percent of ultra low crystallinity fractions, said ultra low crystallinity fractions being defined as the difference between the amount of xylene soluble components as determined at 20°C and 2 hours settling time and the amount of xylene soluble components as determined at 20°C and 5 days settling time.

21. (Original) The composition of claim 13, having a melt flow rate at 230°C and 2.16 kg of between 2 and about 15 g/10 min.

22. (Original) The composition of claim 13, wherein both random copolymers of the polymer blend were prepared by means of a metallocene catalyst.

23. (Original) A film having at least one layer fabricated from the composition of claim 13.

24. (Original) The film of claim 23, wherein the amount of hexane extractable fraction of the film layer comprises no more than about 3.0 weight percent.

25. (Cancelled)

26. (Cancelled)

27. (Previously Presented) A process for preparing a polypropylene composition comprising:

a) providing a catalyst comprising a metallocene compound having the formula

 $R^9L^1L^2M^1R^1R^2$ (Formula I)

wherein

M¹ is a metal of Group IVb of the Periodic Table of the Elements, L¹ and L² are identical or different and are each a substituted mononuclear or polynuclear hydrocarbon radical or (a) hetero atom(s) containing hydrocarbon radical(s), which form a sandwich structure with the central atom M¹,

R¹ and R² are identical or different and are each a hydrogen atom, an alkyl group of from 1 to about 10 carbon atoms, an alkoxy group of from 1 to about 10 carbon atoms, an aryl group of from 6 to about 20 carbon atoms, an aryloxy group of from 6 to about 10 carbon atoms, an alkenyl group of from 2 to about 10 carbon atoms, an OH group, a halogen atom, or a NR₂³² group, where R³² is an alkyl group of from 1 to about 10 carbon atoms or an aryl group of from 6 to about 14 carbon atoms, or R¹ and R² together can form one or more ring system(s),

R⁹ is a bridge between the ligands L.¹ and L.² selected from the groups

wherein R⁴⁰, R⁴¹ can be identical or different, even when they have the same index, and are each a hydrogen atom, a halogen atom or a C₁-C₄₀ group such as a C₁-C₂₀-alkyl group, a C₁-C₁₀-fluoroalkyl group, a C₁-C₁₀-alkoxy group, a C₆-C₁₄-aryl group, a C₆-C₁₀-fluoroaryl group, a C₆-C₁₀-aryloxy group, a C₂-C₁₀-alkenyl group, a C₇-C₄₀-arylalkyl group, a C₇-C₄₀-alkylaryl group or a C₈-C₄₀-arylalkenyl group, where R⁴⁰ and R⁴¹ may each, together with the atoms connecting them, form one or more rings, and z is an integer from zero to 18,

M¹² is silicon, germanium or tin, and

- R⁹ may also link two units of the formula II to one another;
- b) providing a first monomer mixture of propylene and at least one C_2 - C_{20} nonpropylene α olefin in amounts such that the copolymer produced therefrom has a ratio of between 90
 and about 99.5 wt% propylene units to between about 0.5 wt% and 10 wt% of the nonpropylene α -olefin units;
- c) polymerizing the first monomer mixture in the presence of the metallocene catalyst under polymerization reaction conditions to form a first random copolymer having a melting point between 116°C and 145°C;
- d) providing a second monomer mixture of propylene and at least one C_2 - C_{20} nonpropylene α -olefin in amounts such that the copolymer produced therefrom has a ratio of between 85 and about 97 wt% propylene units to between about 3 wt% and 15 wt% of the non-propylene α -olefin;
- e) polymerizing the second monomer mixture in the presence of the metallocene catalyst under polymerization reaction conditions to form a second random copolymer having a melting point between 70°C and 116°C; and
- f) blending the first random copolymer and the second random copolymer to provide a polypropylene copolymer composition including about 60 wt% to about 95 wt% of the first random copolymer and from about 5 wt% to about 40 wt% of the second random copolymer based upon total composition weight;
- wherein said polymer blend includes a fraction soluble in xylene at 20°C, determined at 20°C and 5 days settling time, the xylene soluble fraction having a weight average

molecular weight of more than 100 kg/mol and an intrinsic viscosity of above about 1.0 dl/g.

28. (Original) The process of claim 27 where the catalyst comprises a metallocene compound having the formula

(Formula II)

wherein

M¹ is zirconium or hafnium

R¹, R², and the bridging unit R⁹ have the meaning set forth above with respect to formula I.

R⁴, R⁵, R⁶, R⁷, R⁸ and also R⁴, R⁵, R⁶, R⁷ and R⁸ are identical or different and are each a hydrogen atom, a linear, cyclic or branched hydrocarbon group, with or without heteroatoms, selected from an alkyl group of from 1 to about 10 carbon atoms, an alkenyl group of from 2 to about 10 carbon atoms, an aryl group of from 6 to about 20 carbon atoms, an arylalkyl group of from 7 to about 40 carbon atoms, an alkylaryl group of from 7 to about 40 carbon atoms, a substituted or unsubstituted alkylsilyl or arylsilyl group and/or two adjacent

radicals R⁵, R⁶ or R^{5'}, R^{6'}, or R⁶, R⁷ or R^{6'}, R^{7'}, or R⁷, R⁸ or R^{7'}, R^{8'} in each case may form a hydrocarbon ring system or R⁵ and R^{5'} are identical or different and are each a substituted or unsubstituted aryl group of from 6 to about 40 carbon atoms.

- 29. (Original) The process of claim 27, wherein the polymerizing steps (c) and (e) are performed using a reactor cascade composed of at least two reactors in series.
- 30. (Original) The process of to claim 29, wherein the polymerization is carried out in gas phase.
- 31. (Original) The process of claim 27 using hydrogen in polymerization steps (c) and/or (e) as a molecular weight regulator.
- 32. (Original) The process of claim 27 wherein the metallocene compound is selected from the group consisting of
 - dimethylsilandiyl(2-methyl-4-(para-tert-butyl-phenyl)-indenyl)(2-isopropy- l-4-(para-tert-butyl-phenyl)-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-ethyl-4-(4'-tert.butyl-phenyl)-indenyl)(2-isopropyl-4- -(4'-tert.-butyl-phenyl)-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-methyl-4-(4'-tert.butyl-phenyl)-indenyl)(2-isopropyl-- 4-phenyl-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-methyl-4-phenyl)-1-indenyl)(2-isopropyl-4-(4'-tert.-b- utyl-phenyl)-1-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-ethyl-4-(4'-tert.butyl-phenyl)-indenyl)(2-isopropyl-4- -phenyl)-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-isopropyl-4-(4'-tert.butyl-phenyl)-indenyl)(2-methyl-- 4,5-benzo-indenyl)zirconiumdichloride,
 - dimethylsilandiyl(2-methyl-4-(4'-tert.butyl-phenyl)-indenyl)(2-isopropyl-- 4-(1-naphthyl)-indenyl)zirconiumdichloride and

dimethyl silandiyl (2-isopropyl-4-(4'-tert.butyl-phenyl)-indenyl) (2-methyl4--(1-naphthyl)-indenyl) (2-methyl4--(1-naphthyl4--(1-naphthyl)-indenyl) (2-methyl4--(1-napht